

**Cover Letter and Notice of Alteration
Assessment - Removal of Chiller
Minnedosa Ethanol Plant
Manitoba Conservation License No. 2698R**

May 2022

SENT ELECTRONICALLY (EABDirector@gov.mb.ca)

Director, Environmental Approvals Branch
Manitoba Environment Climate and Parks
1007 Century Street
Winnipeg, MB R3H 0W4

Attn: Director

**Re: Cenovus (formerly Husky Oil Operations Limited)
Minnedosa Ethanol Plant
Manitoba Conservation Licence No. 2698R
Proposed Alterations to Ethanol Plant – Chiller Removal**

Introduction

Cenovus Energy Inc (Cenovus) acquired the Minnedosa Ethanol Plant from Husky Oil Operations Ltd in Q1 2021. Since that time a review of the plants process has been completed and a decision has been made to remove the chillier unit (CH-409). This letter report provides the necessary background information and rational to support a Notice of Alteration (NOA) to amend the existing approval to accommodate this process change. Cenovus is working with Manitoba Environment Climate and Parks to complete the transfer of approval 2698R from Husky Oil Operations Ltd.

Removal of the chiller will improve environmental outcomes and reduce operating costs. However, during plant shutdowns (3 times per year) the temperature of fluid entering the absorber will for a short time not be in compliance with license condition 26. Therefore, Cenovus requires an amendment to the license to allow for this process change to occur (see below).

A detailed explanation of the proposed alteration and license amendment request follows. Figure 1 provides a high-level summary of the existing and proposed processes. The proposed process flow diagram is presented in Attachment A.

With approval from Manitoba Environment Climate and Parks a pilot program to evaluate this process change has been completed. This pilot program confirmed that the process change will not result in a decrease in ethanol recovery and that ethanol recovery increases as the temperature of the condensate inlet temperature decreases.

Project Background

The Minnedosa ethanol plant (MEP) is located on several parcels of industrial zoned land in the Town of Minnedosa, Manitoba. The MEP began operation in 2005 and has undergone amendments in 2005, 2011, 2012 and 2016. The facility operates under Manitoba Energy Climate and Parks approval 2698R.

The absorber (T-406) is currently equipped with a process chiller (CH-409) to cool the processes condensate stream to the absorber at a temperature low enough to comply with the environmental license for MEP (12°C to 30°C). For economic and reliability reasons, we are proposing to decommission the chiller and use potable town water instead that is consistently at a temperature of about 8°C. The current chiller uses a 110 HP motor with high electricity usage in addition to high annual maintenance costs.

To achieve the cooling demonstrated by the chiller, potable town water at 8°C passes through the heat exchangers to cool the process flow for the absorber. The heated town water will then be pumped into the potable water source header for use in the Utilities building. By sending the heated town water to utilities, the system will require less natural gas to heat the reverse osmosis (RO) permeate water for use in the boiler (BR-1700).

The primary operating savings are associated with reduced electricity and natural gas consumption and elimination of the chiller maintenance costs. From an environmental outcome perspective, the process change will not result in increased water use or wastewater generation and there will be a reduction in green house gas emissions.

Project Description

Figure 1 provides a description of the new ethanol recovery process. The project scope includes the removal of the chiller (CH-409) and minor changes to process piping to (1) re-route the absorber effluent (T-406) directly to heat exchanger E-408 and (2) direct heated Town water from heat exchangers E-408 and E-418 to the Utilities building. No additional tankage or additional process modifications will be required. The new process flow diagrams are provided in Attachment A.

During plant shutdowns (approx. 3 times per year) the water demand approaches zero; however, for a short period of time (up to 48 hours) after shutdown the absorber is still operational, and water is required to ensure efficient CO₂ capture. During this time Cenovus is proposing to directly run Town water into the absorber at a rate of approximately 5.0m³/h for up to 48 hours. This minimizes overall water use and wastewater generation. This additional wastewater generation (~500 m³) offsets the increased capture of CO₂ during these shutdown periods.

Potential Environmental and Community Effects From Process Change

Impacts to the following aspects were considered for the chiller replacement project.

Environmental Aspect	Discussion of Potential Impact
Water Use	No additional water use required during normal operations. Additional small volumes would be required over the short-term during plant turnarounds or other plant shutdowns
Process Emissions	No additional emissions from previously approved.
Terrestrial Biota	None. No new footprint is required.
Socioeconomic Environment	None. Project does not significantly change plant operations.
Noise	None. Minimal increase in noise during construction
Odours	None. No change from previously approved
Light	None. No change from previously approved
Traffic	None. There may be a temporary difference in traffic during construction
Air Quality	None. No change from previously approved. Project will reduce electricity and natural gas consumption.

Environmental benefits from removing the chiller from the process include:

- During normal operations there will be no increase in freshwater use or wastewater generation.
- An annual reduction in electricity consumption of 450,000 kwh.
- An annual reduction of 33,000 m³ of natural gas consumption.

NOA Requested Change to License

Condition 26 of the license prohibits the condensate stream inlet temperature to be below 12°C. Therefore, to facilitate the proposed process change Cenovus is requesting that condition 26 be amended to allow for the temperature of the liquid stream entering the absorber to not exceed 30°C rather than the existing temperature range (i.e., 12°C to 30°C). With this proposed change, Condition 26 would read as follows:

26. The licensee shall install, calibrate, maintain and operate the ethanol absorption column according to manufactures specifications and shall install, calibrate, maintain and operate temperature indicators to monitor the temperature of the liquid streams in the ethanol absorber. The ethanol absorber column shall be operated so that the temperature of the condensate stream entering the absorber does not exceed 30°C.

Project Schedule

Project activities are anticipated to begin with civil construction starting in September with a projected startup of early October 2022.

Closure

The proposed project results in improved ethanol recovery with no increase in water use or wastewater generation but significant decreases in electricity and natural gas consumption.

If you have any questions, or if you require any further information, please do not hesitate to contact Scott Hillier at 403-766-7356 or at scott.hillier@Cenovus.com .

Sincerely,



Scott Hillier, M.Sc., P. Eng. (AB)
Regulatory Services



Mounir Nasser, E.I.T
Staff Project Engineer
Downstream and Midstream Projects

Attachments

Attachment A: Process Flow Diagram

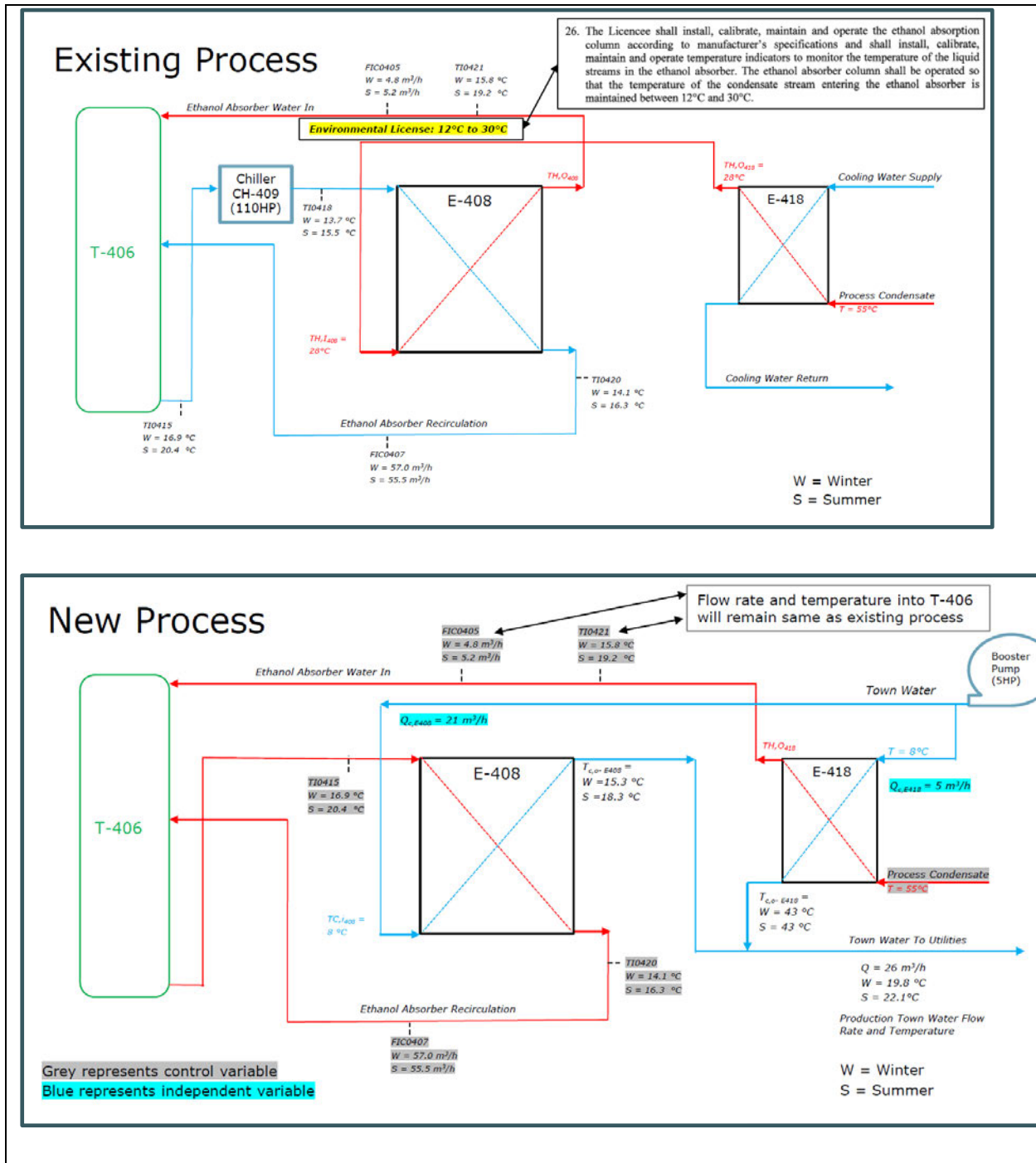
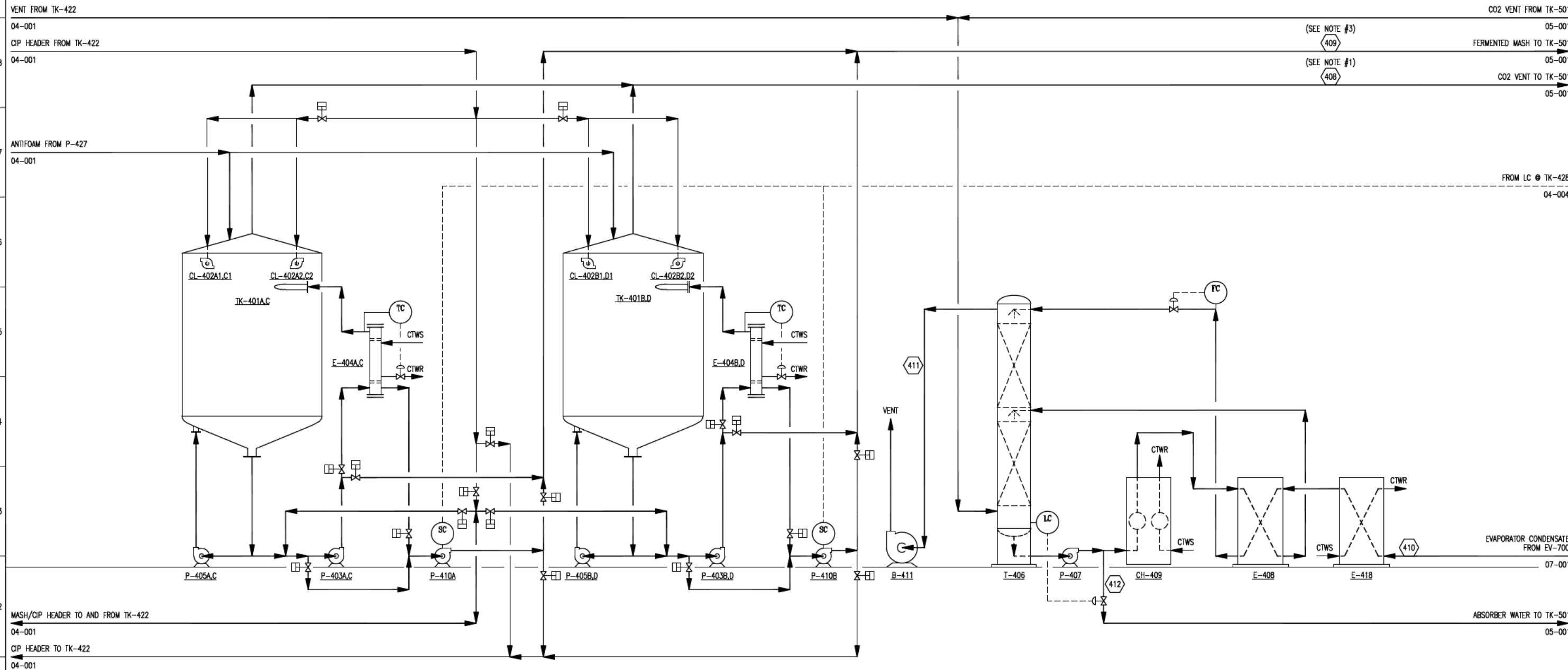


Figure 1 - Diagram Showing Existing and Proposed Process Changes Near the Absorber (T-406)

Attachment A

STREAM NUMBER	DESCRIPTION	408 FERMENTER VENTS	409 BEER	410 EVAPORATOR CONDENSATE	411 ABSORBER VENT	412 ABSORBER WATER
COMPONENT, mass%						
WATER		2.33	78.95	98.99	0.71	92.02
ETHANOL		0.94	8.99	0.21	0.00	3.94
CARBON DIOXIDE		95.83	0.08	0.00	98.28	4.33
HEADS		0.01	0.00	0.00	0.01	0.01
FUSEL OILS		0.00	0.00	0.00	0.00	0.00
FERMENTABLE SOLIDS		0.00	0.00	0.00	0.00	0.00
NON-FERMENTABLE SOLIDS		0.00	11.97	0.00	0.00	0.00
TOTAL, bbl/hr		29.645	311.422	7.998	29.201	8.244
TOTAL, kg/hr		13,447	141,259	3,628	13,245	4,193
TEMPERATURE, °F (°C)		95 (35)	95 (35)	121 (49)	59 (15)	62 (17)
PRESSURE, psig (kPa)		0 (0)	35 (243)	35 (243)	0 (-3)	52 (361)
LIQUID FLOW, gpm (bbl/hr)			604.7 (2289.1)	16.2 (61.2)		18.9 (71.4)
GAS FLOW, acfm (m ³ /hr)		4673 (7939)			4364 (7397)	



P-405A.C FERMENTER CIRCULATION PUMPS	CL-402A1.C1 FERMENTER CLEANERS	TK-401A.C FERMENTERS	CL-402A2.C2 FERMENTER CLEANERS	P-403A.C FERMENTER PUMPS	E-404A.C FERMENTER COOLERS	P-410A CIP RETURN PUMP	P-405B.D FERMENTER CIRCULATION PUMPS	CL-402B1.D1 FERMENTER CLEANERS	TK-401B.D FERMENTERS	CL-402B2.D2 FERMENTER CLEANERS	P-403B.D FERMENTER PUMPS	E-404B.D FERMENTER COOLERS	P-410B CIP RETURN PUMP	B-411 ETHANOL ABSORBER BLOWER	T-406 ETHANOL ABSORBER	P-407 ETHANOL ABSORBER CIRCULATION PUMP	CH-409 PROCESS WATER CHILLER	E-408 ETHANOL ABSORBER COOLER	E-418 PROCESS WATER COOLER
---	--------------------------------------	-------------------------	--------------------------------------	--------------------------------	----------------------------------	---------------------------------	---	--------------------------------------	-------------------------	--------------------------------------	--------------------------------	----------------------------------	---------------------------------	--	------------------------------	---	---------------------------------------	--	-------------------------------------

- NOTES:
1. FERMENTER VENT STREAMS EQUAL AVERAGE FOR ALL FOUR (4) FERMENTERS.
 2. HEAT DUTY SHOWN IS AT PEAK CONDITION, AND IS THE COMBINED DUTY FOR THE SYSTEM.
 3. FLOW RATES SHOWN ARE TIME-AVERAGED VALUES. INTERMITTENT FLOW IS GREATER.
 4. MATERIAL BALANCE IS SHOWN FOR KEY PROCESS STREAMS AT STEADY STATE. MATERIAL BALANCE DOES NOT INCLUDE STREAMS THAT ARE INTERMITTENT, INDETERMINATE, OR NORMALLY ZERO. VENTS FROM EQUIPMENT CONTAINING SUBCOOLED LIQUID HAVE ZERO FLOW AT STEADY STATE.

The process design and other information contained on this drawing is the property of KATZEN INTERNATIONAL, INC. Confidential. This and may not be reproduced in any manner, discussed with, or submitted in any confidential person or organization, without prior written approval by an authorized representative of KATZEN INTERNATIONAL, INC. KATZEN INTERNATIONAL, INC. is authorized to practice engineering in the state of Ohio, USA. All note requirements shall be reviewed by a person or persons licensed to practice engineering in the applicable jurisdiction, unless stipulated otherwise.

PRINT ISSUED
9/30/05
CONFIDENTIAL

#	DESCRIPTION	BY	DATE	APPD.

KATZEN INTERNATIONAL, INC.
TECHNOLOGY • ENGINEERING CINCINNATI, OHIO, U.S.A.

HUSKY OIL LIMITED
MINNESOTA, MANITOBA, CANADA

130 MM LPY WHEAT TO MERGE PROJECT POP
PROCESS FLOW DIAGRAM

SECTION 400 - FERMENTATION AND CIP SYSTEM - SHEET 2 OF 4

ORIGIN:	DRAWN:	CHECKED:	DATE:	SCALE:	CLIENT No.:	DWG. No.:	REV.
TNV	RLM	TNV	3/31/05	NONE	998-09	04-002	0