ELCANO EXPLORATION INC.



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August 1, 2019

Manitoba Growth, Enterprise and Trade Petroleum Branch Box 1359, 590 Wellington Street East Virden, MB R0M 2C0

Attention: Petroleum Inspectors

RE: Application for an Oil Battery Permit 02-27-012-27WPM

Elcano Exploration Inc. (Elcano) respectfully submits an application for an oil battery permit under Part 7, section 111(2) of *The Oil and Gas Act* and Part 7, section 75(1) of the *Drilling and Production Regulation*.

As per the section 75(1) of the Drilling and Production Regulation, the following information is provided as part of this application:

- a. the application fee and levy;
- b. the performance deposit;
- c. a survey plan of the battery location;
- d. the names and addresses of all landowners and occupants within 1.5 km of the proposed site of the battery and the applicant's consultations with those landowners and occupants, any concerns raised during the consultation process and all actions taken or proposed to be taken by the applicant to address the concerns of the landowners and occupants;
- e. an estimate of the production rates of oil, water and gas for the battery, including the estimated volume of gas
 - i. used for fuel,
 - ii. flared, or
 - iii. vented;
- f. a representative gas analysis for the battery;
- g. the specifications of any process vessel to be used;
- h. details of well testing facilities associated with the battery;

- i. details of the flare and vapour recovery systems for the battery;
- j. proposal to vent gas containing hydrogen sulphide,
 - i. reasons why the gas cannot be flared,
 - ii. specific actions to be taken to minimize the volume of gas vented, and
 - iii. the method of controlling off-lease odours;
- k. where gas production will contain hydrogen sulphide, a copy of air dispersion modelling results demonstrating that the battery will comply with;
- l. a plot drawing on a scale of not less than 1:125 and showing the location of
 - i. each process vessel, tank and salt water disposal facility,
 - ii. any pit, dyke, flare line or pop tank, and its size, and
 - iii. any other equipment;
- m. a schematic process flow diagram showing
 - i. process vessels, meters, tanks and salt water disposal equipment,
 - ii. valves, pumps and piping,
 - iii. pressure relief valves and settings, emergency shut down systems, and any other equipment intended to prevent a spill or to mitigate the amount of a spill;
- n. plans for the disposal of produced water; and
- o. any other information that an inspector or the director may require.

Should you have any questions or concerns, please contact me at 403.930.7681

Sincerely,

ELCANO EXPLORATION INC.

Darren Rennie, P. Eng

Vice President Engineering & COO

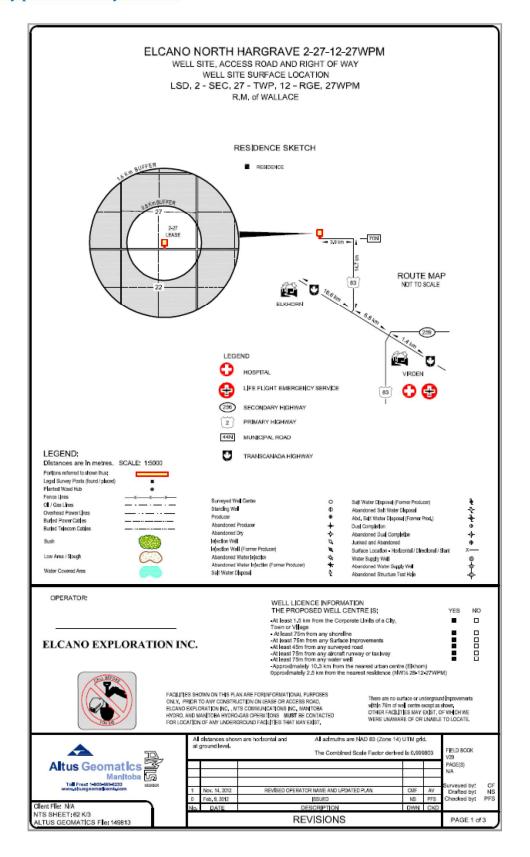
a. Application fee and levy

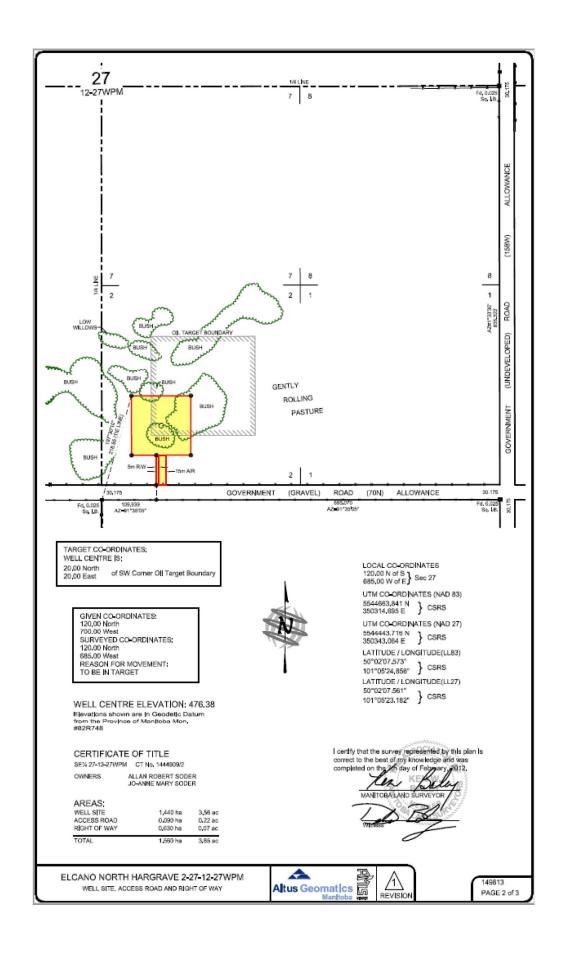
The application fee (\$750) and levy (\$250) has been mailed in the form of a cheque, payable to the Minister of Finance.

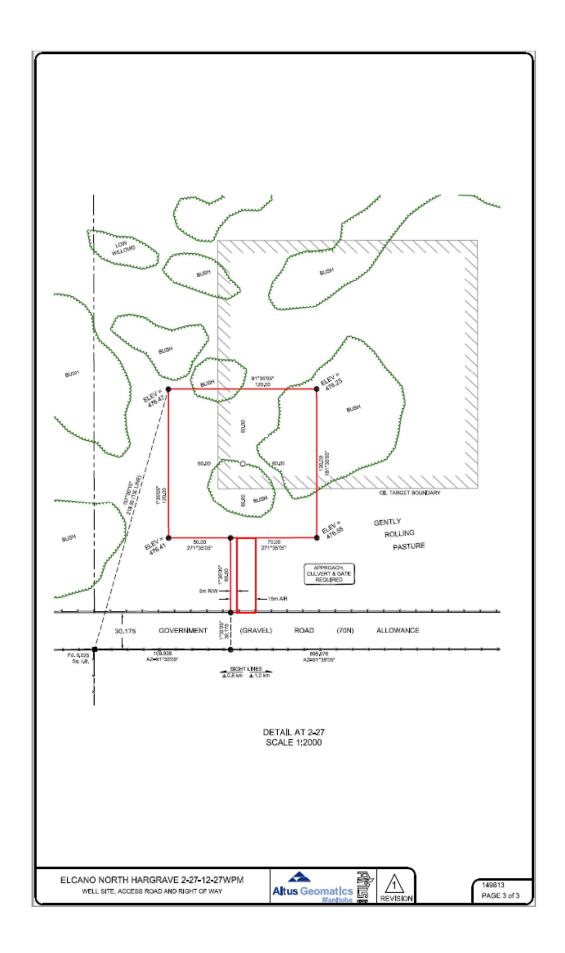
b. Performance deposit

No additional performance deposit is required to obtain this battery operating permit

c. Survey plan of battery location







e. <u>An estimate of the production rates of oil, water and gas for the battery, including the estimated volume of gas used for fuel, flared or vented</u>

The anticipated daily volumes entering the proposed 02-27 battery:

0il: $60 \text{ m}^3/\text{d}$ Water: $3000 \text{ m}^3/\text{d}$

Gas: $300 \text{ m}^3/\text{d} \text{ (GOR at 5 m}^3/\text{m}^3\text{)}$

The above gas rate is used to create the dispersion modelling. All of the gas on site will be gathered through a vapour recovery unit and flared through flare stack.

f. A copy of a representative gas analysis for the battery



GAS ANALYSIS

| | | | | | | | | GA. | ANALTSIS | | |
|---|-------------|---------------------|------------------|---------------------------|---------------------------|--|-----------------------------------|--|---------------------------------------|--|--|
| TB1A | | | | | | | | 1 | 6GS074435A | | |
| Container Identification Sample Point Code Meter Code | | | | AGAT | AGAT WDMS Number Previous | | Number Laboratory Number | | | | |
| EL CANO EX | | NI TO | | | ELADE STAC | V | | 03_3/_01 | 2-27\/\/1 | | |
| ELCANO EXPLORATION LTD Operator Name | | | | | Sampling Point | FLARE STACK Sampling Point | | | 03-34-012-27W1 Unique Well Identifier | | |
| NODTH HA | | A DATTEDY | | | | | | | | | |
| Well Name | RGRAVE 3-3 | 34 BATTERY | 14/- | Il License Wei | II Ctatus | MAN EA | id Status | LSD | | | |
| well Name | | | we | ir License Wei | ii Status | well Flu | id Status | LSD | | | |
| NORTH HAI | RGRAVE | | NOT APPL | CABLE | | AGAT/ESTE | | JS/JV | | | |
| Field or Area | | F | ool or Zone | | Elevation (m) | Sampler's Comp | any Pressure (kPa) - | Name of Sa | mpler 「emperature (°C) ——— | | |
| Test Inter | vai (mk.B) | | | | | 1 | resoure (m a) | | | | |
| From | То | Test Type | Test | No. | KB GRI | | e Recei | | | | |
| Mar 07, 2016 | 6 Mar | | Mar 17. | 2016 | Mar 17, 2016 | Calgan | / - Gerny Ec | ker - Reporter | | | |
| Date Sampled | | Received | Date Analy | | Date Reported | | Approved By - | | | | |
| Other FIE Information | LD H2S BY | TUT = 7.88% | | | | | | | | | |
| | | COMPOS | NTION | | | | PROPER | TIES | | | |
| | | COMPOS | SITION | | Calcula | ted Heating V | /alue @ 15 9 | C & 101 335 | kDa /M I/m³) | | |
| | Mole F | raction | | | Calcula | ted Heating V Gross | alue @ 15 | | Net | | |
| | Air Free | Air & Acid Gas | Liquid Volume | Mole Fraction of Previous | 66.13 | 78.97 | 1.02 | 60.24 | 71.95 | | |
| Component | As Received | Free As Received | mL/m³ | Analysis | Air Free as | Moisture & | C ₇ + Moisture | Air Free as | Moisture & | | |
| H ₂ | TRACE | TRACE | | | Received | Acid Gas Free | Free | Received | Acid Gas Free | | |
| He | 0.0010 | 0.0012 | | | Calculated Density | | | | | | |
| N₂ | 0.1182 | 0.1453 | | | 11 | Relative | 0.574 | 200.0 | Absolute | | |
| CO ₂ | 0.1079 | 0.0000 | | | 1.401 Moisture Free | 1.407 Moisture & Acid | 3.571 | 692.6 | 1.716 Total Sample | | |
| H₂S | 0.0788 | 0.0000 | | | As Received | Gas Free | C ₇ + Moisture Free | C ₇ + Density (kg/m²) | Density (kg/m²) | | |
| C ₁ | 0.0309 | 0.0380 | | | | Calculated I | Pseudo Crit | ical Propertie | es — | | |
| C ₂ | 0.2277 | 0.2800 | 809.2 | | A | s Sampled | Î | Acid | Gas Free | | |
| C ₃ | 0.2607 | 0.3205 | 958.0 | | 4897.6 | 324.7 | | 4171.3 | 322.7 | | |
| iC₄ | 0.0539 | 0.0663 | 235.4 | | pPc (kPa) | DTc (K) | _ | pPc (kPa) | pTc (K) | | |
| nC ₄ | 0.0788 | 0.0969 | 331.5 | | | | | A/ 5 - 5 - 7 - 6 - 7 - 7 | | | |
| iC₅ | 0.0218 | 0.0268 | 106.4 | | | — Hydrog | en Sulfide (| (H₂S) (ppm) | | | |
| nC ₅ | 0.0086 | 0.0106 | 41.6 | | Field | <i>Value</i> | Lab | oratory Value | g/m³ | | |
| Се | 0.0069 | 0.0085 | 37.9 | | | 78800 | | | 113.36 | | |
| C ₇ + | 0.0048 | 0.0059 | 30.4 | | Stain Tube | Tutweiler | Other | GC-SCD | _ | | |
| TOTAL | 1.0000 | 1.0000 | 2550.4 | | | Calcula | ted Molecu | lar Weight | | | |
| | | | | | | | | eived) (g/mol |) | | |
| | | | | | 40.6 | | | 103.4 | | | |
| | | | | | Total S | ample | | C ₇ + Fraction | 7 | | |
| WDMS Data Verification Check | | | | | Calculat | Calculated Vapour Pressure Gas Compressibility | | | | | |
| Exceeds normal limits :IC5, N2 | | | | | 101.6 | 101.62 0.9819 | | | | | |
| | | | | | C ₃ + (kP | | @15 °C & 101.325 kPa | | | | |
| | | | | | - | | | | | | |

g. The specifications of any process vessel to be used

The configuration of the battery will be such that only atmospheric tanks will be used for processing emulsion. No vessels operating above atmospheric pressure will be used in any part of the proposed 02-27 facility.

h. Details of well testing facilities associated with the battery

Each well is to be tested by a mobile production test unit on a monthly basis. The production testing unit will be deployed to each wellsite to conduct a minimum 24 hour production test. Well head samples will be taken during the test period to determine representative oil and water cuts.

i. Details of the flare and vapour recovery systems for the battery

All gas flashed off within the processing tanks will be collected through a vapour recovery system and directed to a flare system. Any atmospheric vents will be fitted with H₂S scrubbers.

j. Proposal to vent gas containing hydrogen sulphide

Since all gas collected will be directed to a flare system, there will be no intentional venting of gas to the atmosphere. As well, H_2S scrubbers will be installed where necessary to further prevent any off lease odours.

k. Air dispersion modelling

Using the Screen3 Emissions Modelling software, the maximum 1 hour concentration from flaring emissions for SO_2 flare is $100.2~\mu g/m^3$ at 260~m. This meets the requirements as defined in Subsection 85.2(1), Schedule G in the Manitoba Drilling and Production Regulations is within the defined limits. The Screen3 model inputs and outputs are below

Air dispersion modelling inputs:

Company: Elcano Exploraiton Inc. Facility: Battery 02-27-012-27W1M

| Gas Stream | To Flare | |
|--|---------------|-------------------|
| Flow Rate | 0.300 | 10³ m³/d |
| Percentage | 100.0 | % |
| Reference Temp | 15 | °C |
| | | |
| Flare Gas Stream | Mole Fraction | |
| H ₂ | 0.0000 | |
| He | 0.0010 | |
| N ₂ | 0.1182 | |
| CO ₂ | 0.1079 | |
| H ₂ S | 0.0788 | |
| C_1 | 0.0309 | |
| C ₂ | 0.2277 | |
| C₃ | 0.2607 | |
| i C ₄ | 0.0539 | |
| n C ₄ | 0.0788 | |
| i C ₅ | 0.0218 | |
| n C₅ | 0.0086 | |
| C ₆ | 0.0069 | |
| | 0.0009 | |
| C ₇ + Total | 1.0000 | |
| Iotal | 1.0000 | |
| Gas Stream Properties | | |
| Molecular Mass | 40.5852 | g/mole |
| Net Heating Value | 66.1300 | MJ/m ³ |
| Net Heat Release Rate | 54880 | cal/s |
| | | ,- |
| Stack Parameters | | |
| Flare Stack Height | 12.2000 | m |
| Flare Stack Diameter | 0.0760 | m |
| Actual Exit Velocity | 0.7654 | m/s |
| Length of Flame | 0.8402 | m |
| Conversion Efficiency | 100.00% | % |
| NO DECEMBER OF THE PARTY OF THE | | |
| Model Input Parameters | | |
| Gas Flow Rate | 0.0035 | m ³ /s |
| Effective Stack Height | 13.0402 | m |
| Exit Temperature | 1273 | K |
| Ambient Temperature | 273 | K |
| entatura. | | |
| Emissions | 0744257 | -/- |
| SO ₂ Emissions | 0.741267 | g/s |
| H ₂ S Emissions | 0.000000 | g/s |

Air dispersion modelling outputs:

08/01/19 15:53:12

```
*** SCREEN3 MODEL RUN ***

*** VERSION DATED 13043 ***
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C:\Users\drennie\Documents\Engineering\Screen3 View\Models\02-27 Battery - 0716

SIMPLE TERRAIN INPUTS:

| SOURCE TYPE | = | FLARE |
|------------------------|---|----------|
| EMISSION RATE (G/S) | = | 0.741267 |
| FLARE STACK HEIGHT (M) | = | 12.2000 |
| TOT HEAT RLS (CAL/S) | = | 54880.0 |
| RECEPTOR HEIGHT (M) | = | 0.0000 |
| URBAN/RURAL OPTION | = | RURAL |
| EFF RELEASE HEIGHT (M) | = | 13.0402 |
| BUILDING HEIGHT (M) | = | 0.0000 |
| MIN HORIZ BLDG DIM (M) | = | 0.0000 |
| MAX HORIZ BLDG DIM (M) | = | 0.0000 |

THE REGULATORY (DEFAULT) MIXING HEIGHT OPTION WAS SELECTED. THE REGULATORY (DEFAULT) ANEMOMETER HEIGHT OF 10.0 METERS WAS ENTERED.

BUOY. FLUX = 0.910 M**4/S**3; MOM. FLUX = 0.555 M**4/S**2.

*** FULL METEOROLOGY ***

*** TERRAIN HEIGHT OF 0. M ABOVE STACK BASE USED FOR FOLLOWING DISTANCES ***

| DIST | CONC | CEAD | U10M | USTK | | PLUME | SIGMA | SIGMA | DEED CH |
|-------|-----------|------|-------|-------|---------|--------|-------|-------|---------|
| (M) | (UG/M**3) | STAB | (M/S) | (M/S) | (M) | HT (M) | Y (M) | Z (M) | DWASH |
| 5. | 0.000 | 1 | 1.0 | 1.0 | 320.0 | 32.63 | 2.20 | 1.51 | NO |
| 100. | 83.12 | 1 | 2.0 | 2.0 | 640.0 | 22.84 | 27.00 | 14.23 | NO |
| 200. | 95.21 | 3 | 2.0 | 2.1 | 640.0 | 22.76 | 23.78 | 14.30 | NO |
| 300. | 97.39 | 3 | 1.5 | 1.5 | 480.0 | 26.00 | 34.49 | 20.66 | NO |
| 400. | 91.78 | 3 | 1.0 | 1.0 | 320.0 | 32.48 | 44.99 | 27.02 | NO |
| 500. | 85.55 | 4 | 1.5 | 1.6 | 480.0 | 25.83 | 36.33 | 18.66 | NO |
| 600. | 81.48 | 4 | 1.0 | 1.0 | 320.0 | 32.22 | 43.07 | 21.91 | NO |
| 700. | 79.10 | 4 | 1.0 | 1.0 | 320.0 | 32.22 | 49.49 | 24.65 | NO |
| 800. | 74.15 | 4 | 1.0 | 1.0 | 320.0 | 32.22 | 55.84 | 27.34 | NO |
| 900. | 68.32 | 4 | 1.0 | 1.0 | 320.0 | 32.22 | 62.13 | 29.97 | NO |
| 1000. | 62.44 | 4 | 1.0 | 1.0 | 320.0 | 32.22 | 68.35 | 32.56 | NO |
| 1100. | 57.01 | 4 | 1.0 | 1.0 | 320.0 | 32.22 | 74.51 | 34.56 | NO |
| 1200. | 52.18 | 4 | 1.0 | 1.0 | 320.0 | 32.22 | 80.63 | 36.51 | NO |
| 1300. | 47.90 | 4 | 1.0 | 1.0 | 320.0 | 32.22 | 86.69 | 38.39 | NO |
| 1400. | 44.11 | 4 | 1.0 | 1.0 | 320.0 | 32.22 | 92.71 | 40.23 | NO |
| 1500. | 40.74 | 4 | 1.0 | 1.0 | 320.0 | 32.22 | 98.69 | 42.03 | NO |
| 1600. | 38.64 | 6 | 1.0 | 1.2 | 10000.0 | 35.81 | 52.40 | 19.88 | NO |
| 1700. | 39.39 | 6 | 1.0 | 1.2 | 10000.0 | 35.81 | 55.32 | 20.57 | NO |
| 1800. | 39.86 | 6 | 1.0 | 1.2 | 10000.0 | 35.81 | 58.23 | 21.25 | NO |

| 1900. 2000. 2100. 2200. 2300. 2400. 2500. 2600. 2700. 2800. 2900. | 40.10 40.14 39.81 39.39 38.91 38.38 37.81 37.22 36.60 35.97 35.33 34.68 | 6 6 6 6 6 6 6 6 6 6 6 6 | 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 | 1.2 1.2 1.2 1.2 1.2 1.2 1.2 1.2 | 10000.0 10000.0 10000.0 10000.0 10000.0 10000.0 10000.0 10000.0 10000.0 10000.0 10000.0 | 35.81 35.81 35.81 35.81 35.81 35.81 35.81 35.81 35.81 35.81 | 61.13 64.01 66.87 69.73 72.57 75.40 78.22 81.03 83.82 86.61 89.39 92.15 | 21.92 22.58 23.14 23.69 24.23 24.76 25.28 25.79 26.29 26.78 27.27 27.75 | NO NO NO NO NO NO NO NO NO |
|---|--|--|---|--|---|--|--|--|--|
| MAXIMUM 260. | 1-HR CONCENTE 100.2 | RATION AT | OR BE | EYOND 1.5 | 5. M: 480.0 | 26.00 | 30.40 | 18.28 | NO |

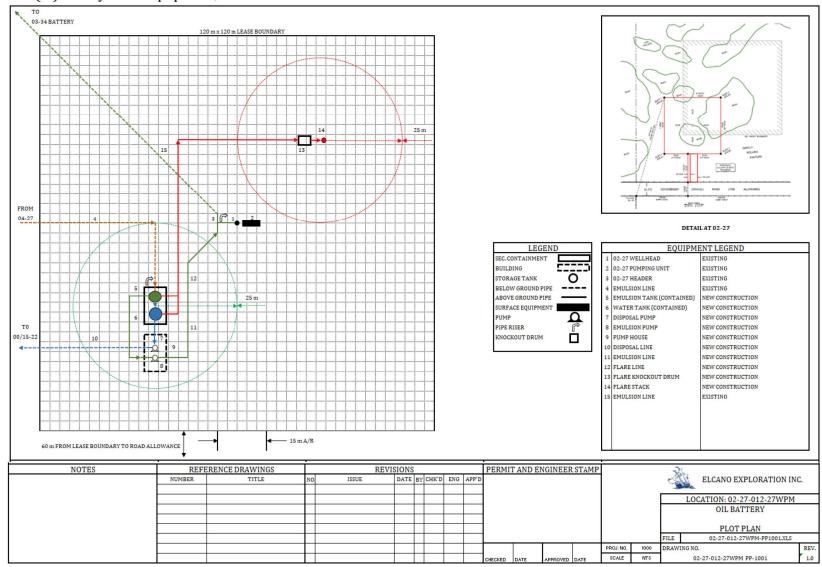
DWASH= MEANS NO CALC MADE (CONC = 0.0)
DWASH=NO MEANS NO BUILDING DOWNWASH USED
DWASH=HS MEANS HUBER-SNYDER DOWNWASH USED
DWASH=SS MEANS SCHULMAN-SCIRE DOWNWASH USED
DWASH=NA MEANS DOWNWASH NOT APPLICABLE, X<3*LB

**** SUMMARY OF SCREEN MODEL RESULTS ***

| CALCULATION | MAX CONC | DIST TO | TERRAIN |
|----------------|-----------|---------|---------|
| PROCEDURE | (UG/M**3) | MAX (M) | HT (M) |
| | | | |
| SIMPLE TERRAIN | 100.2 | 260. | 0. |

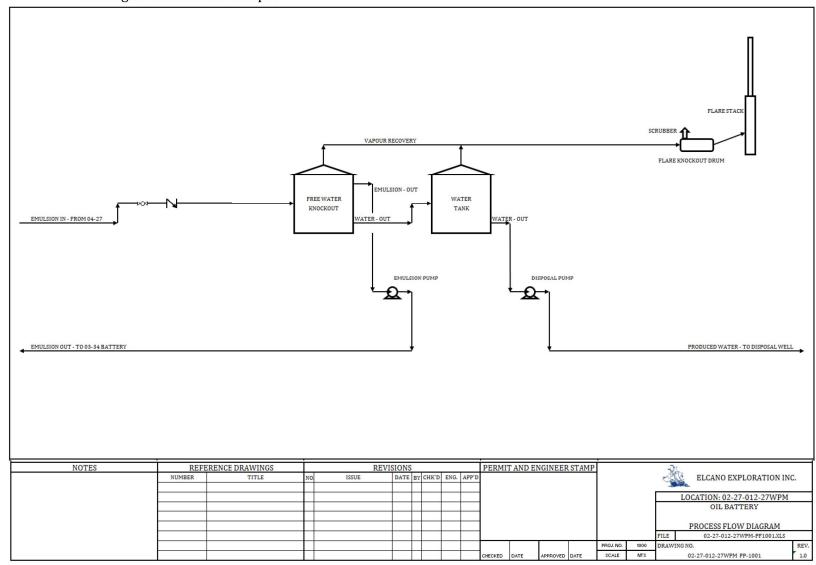
l. A plot drawing showing the location of

- (i) each process vessel, tank and salt water disposal facility
- (ii) any pit, dyke, flare line or pop tank, and its size, and
- (iii) any other equipment;



m. A schematic process flow diagram showing

- (i) process vessels, meters, tanks and salt water disposal equipment,
- (ii) valves, pumps and piping,
- (iii) pressure relief valves and settings, emergency shut down systems, and any other equipment intended to prevent a spill or to mitigate the amount of a spill



n. Plans for the disposal of produced water

The produced water from the battery will be disposed of in the proposed 100/15-22-012-27WPM. A flowline will be constructed from the 02-27 battery to the 15-22 disposal well.

o. Any other information that an inspector or the director may require

Elcano Exploration Inc. is planning to construct a new battery at 02-27-012-27 WPM as part of the continued development in the North Hargrave area.

The proposed battery at 02-27-012-27 WPM will allow Elcano to continue exploitation of existing wells and potential for economic development of new wells in the area. Elcano has reach water handling limitations at its existing 03-34-012-27WPM battery. Careful analysis indicates that a second 'satellite' battery designed to remove and dispose of a majority of water, prior to the 03-34 battery, is the best solution. Remaining emulsion from the 02-27 battery will still be processed for sales quality oil at the 03-34 facility.

The 02-27 facility will be designed to initially process approximately 3,060 m 3 /d of emulsion (3,000 m 3 /d water; 60 m 3 /d oil) assuming the inlet stream is approximately 98% water. Approximately 95% of the water will be removed and the remaining emulsion volume will be transported to the 03-34 facility via existing flowlines for processing to sales quality oil. No fluids will be routinely trucked from this facility. GOR is estimated at 5 m 3 /m 3 , all gas will be recovered through a vapour recovery unit and flared.